# 3D Microstructure of Ni-YSZ anodes: Prediction of effective transport properties and

# optimization of redox stability

Omar M. Pecho<sup>1,2,\*</sup>, Ole Stenzel<sup>1</sup>, Boris Iwanschitz<sup>3</sup>, Philippe Gasser<sup>4</sup>, Matthias Neumann<sup>5</sup>, Volker Schmidt<sup>5</sup>, Michel Prestat<sup>1</sup>, Thomas Hocker<sup>1</sup>, Robert J. Flatt<sup>2</sup>, Lorenz Holzer<sup>1</sup> <sup>1</sup>Institute of Computational Physics, Zurich University of Applied Sciences, 8400 Winterthur, Switzerland <sup>2</sup>Institute for Building Materials, ETH Zurich, 8093 Zurich, Switzerland <sup>3</sup>Hexis SA, 8404 Winterthur, Switzerland <sup>4</sup>ScopeM, Scientific Center for Optical and Electron Microscopy, ETH Zurich, 8093 Zurich, Switzerland

<sup>5</sup>Institute of Stochastics, Ulm University, 89069 Ulm, Germany

# ABSTRACT

This study investigates the influence of microstructure on the effective ionic and electrical conductivities of Ni-YSZ anodes. Fine, medium and coarse microstructures are exposed to redox cycling at 950°C. FIB-tomography and image analysis are used to quantify effective (connected) volume fraction ( $\phi_{eff}$ ), constriction factor ( $\beta$ ) and tortuosity ( $\tau$ ). The effective conductivity ( $\sigma_{eff}$ ) is described as the product of intrinsic conductivity ( $\sigma_0$ ) and the so-called microstructure-factor (M):  $\sigma_{eff}=\sigma_0^*M$ . Two different methods are used to evaluate the M-factor: (1) by prediction using a recently established relationship:  $M_{pred} = \varepsilon \beta^{0.36} / \tau^{5.17}$  and (2) by numerical simulation that provides conductivity, from which the simulated M-factor can be deduced ( $M_{sim}$ ). Both methods give complementary and consistent information about the effective transport properties and the redox degradation mechanism. The initial microstructure has a strong influence on effective conductivities and their degradation. Finer anodes have higher initial conductivities but undergo more intensive Ni-coarsening. Coarser anodes have a more stable Ni-phase but exhibit lower YSZ stability due to lower sintering activity. Consequently, in order to improve redox stability it is proposed to use mixtures of fine and coarse powders in different proportions for functional anode and current collector layers.

# **1. INTRODUCTION**

Solid oxide fuel cells (SOFC) are electrochemical conversion devices that produce electricity directly from oxidizing a fuel (e.g. natural gas, biogas, H<sub>2</sub>). The advantages of SOFCs are a high efficiency, fuel flexibility and low emissions (pollutants and noise).<sup>1,2</sup> However, the materials are exposed to harsh

<sup>&</sup>lt;sup>\*</sup> Corresponding author. e-mail: pech@zhaw.ch

operating conditions, which include high chemical potentials between anode (reducing atmosphere) and cathode (oxidizing) in combination with high temperatures (750 - 950°C). These harsh conditions may reduce the fuel cell lifetime. Especially in conventional Ni-based anodes, so-called redox cycles that occur during shutdown and restart procedures often lead to a harmful degradation. In the present study we thus investigate the relationship between topological parameters (e.g. tortuosity, constrictivity) with effective anode properties (e.g. ionic or electric conductivities).

The electrochemical performance of Ni-YSZ anodes depends on the interplay between different transport processes and the electrochemical reactions at the triple phase boundary (TPB). Oxygen ions are transported through the ion-conducting yttria-stabilized zirconia (YSZ), electrons through the electron-conducting Ni and gas species through the pores, while the electrochemical reaction primarily occurs near the TPB. The fuel oxidation at the TPB includes numerous intermediate steps,<sup>3</sup> which can be summarized into the following net reaction:

$$H_2 + O^2 \rightarrow H_2O + 2e^-$$
 Eq. 1

The associated charge transport and charge transfer reactions provide specific contributions to the area specific resistance (ASR). The ASR contribution of each process depends on both, the relevant intrinsic property (e.g. intrinsic ionic conductivity of YSZ) and on the corresponding morphological characteristics (e.g. volume fraction and tortuosity of YSZ). The combination of intrinsic properties and microstructural characteristics results in a homogeneous effective macro-property (e.g. effective ionic conductivity).

One way to improve the effective properties and the associated electrode performance is to tailor the microstructure. However, the optimization of electrode microstructures is challenging because of the complex interplay between the various processes taking place.<sup>4</sup> The different properties cannot be manipulated independently from each other. In literature strong focus was laid specifically on the improvement of the electrochemical activity, which correlates with the TPB length (i.e. the number of electrochemically active sites). Therefore, the tendency is to develop finer-grained microstructures with higher TPB length.<sup>5</sup> Nevertheless, in order to ensure that the reaction from Eq.1 occurs throughout the anode, all three phases joining at the TBP must constitute a connected network. Thus, for a high anode performance the microstructure must be optimized also in terms of connectivity and effective transport properties of all three phases (Ni, YSZ, pores). In addition, it is not only the initial microstructure which is important for a successful application of the fuel cell technology. For example electrolyte supported SOFCs with open system configuration undergo several reduction-oxidation

(redox) cycles, which often cause degradation of the microstructure and an associated loss of electrochemical performance. Hence, redox stability is an additional quality criterion for such SOFC anodes.<sup>6</sup>

Redox cycles involve reoxidation of Ni to NiO and then again re-reduction back to Ni. The reaction is accompanied by a volume change of about 70%.<sup>5</sup> The oxidation kinetics are controlled mainly by outward diffusion of Ni and inward diffusion of oxygen. During reduction additional pores are formed and thus the overall kinetics is not diffusion-controlled but it rather depends on the kinetics of surface reactions (e.g. formation of mobile hydroxide species). Repeated redox cycling causes an increase of anode thickness, which can be considered as macroscopic swelling or irreversible expansion. It is generally attributed to the fact that volume expansion during reoxidation is not fully reversible during re-reduction, which leads to an increase in porosity throughout the entire anode microstructure.<sup>7</sup> Nevertheless, on the grain scale (i.e. locally) the volume expansion of Ni particles may be reversible after re-reduction. Aside from the macroscopic swelling, also a redistribution and coarsening of Ni occurs during redox cycling.<sup>6</sup> The mobilization of Ni is strongly enhanced by the formation of Ni(OH)<sub>2</sub> species, which have much higher gas saturation pressures compared to Ni and NiO.8 Especially at high temperatures (>700°C) redistribution of Ni (via Ni(OH)<sub>2</sub>) can become very prominent. Thereby, small Ni grains tend to agglomerate in order to minimize surface energy. The coarsening leads to a degradation of electrical conductivity, but also to a loss of TPB and associated electrochemical activity.

In contrast to Ni, YSZ is generally considered as the rigid ceramic backbone of the anode, which provides mechanical stability.<sup>5,6,9</sup> However, it was shown that the ionic conductivity decreases after redox cycling,<sup>6</sup> which may be related to the crystallographic transformations in YSZ at elevated temperatures. Alternatively, it may be due to the fact that the elevated mobility of ionic species (e.g.  $Zr^{4+}$ ) under redox conditions may lead to changes of both, the YSZ microstructure and its intrinsic conductivity.<sup>10-12</sup> Nonetheless, YSZ can also be affected by the stress induced either by the Ni coarsening or by the subsequent reoxidation, which creates mechanical stresses along the weak points of the ceramic backbone.<sup>6</sup>

In order to study the influence of anode microstructure on the performance and redox stability, the relevant topological parameters must be quantified. For this purpose 3D image analysis is required to gain the necessary information on phase connectivity, tortuosity, constrictivity and active TPB length. Using focused-ion beam scanning electron microscopy (FIB-SEM)<sup>13-20</sup> and X-ray tomography<sup>21-26</sup> it is

possible to obtain 3D microstructure data, which can be used to quantitatively describe the anode topological characteristics. Moreover, information gained from 3D microstructure analysis can be used to design anode microstructures with improved effective properties and redox stability. In principle, the controlled materials design includes two steps: 1.) Establishing experimental methods by which the topological parameters can be influenced in the fabrication process (e.g. deposition method, composition, powder fineness, sintering conditions);<sup>27-33</sup> and 2.) Formulating relationships between microstructure properties and effective material properties. In the past, the second relationship was not established on a quantitative level. However, recently this gap was filled by an approach using virtual materials design (VMT).<sup>34</sup> Thereby a large number of virtual 3D microstructures were created by means of spatial stochastic simulations. The corresponding effective properties (i.e. conductivities) were then determined with numerical transport simulations. Using statistical analysis (i.e. error minimization) an empirical equation describing the relationship between topological parameters and effective transport property was obtained (see Eqs. 3, 4). The derivation of this empirical equation is discussed in the next section.

In general, the influence of microstructure on the effective transport property can be given with the following simple relation:

$$\sigma_{eff} = \sigma_0 M \qquad \qquad \text{Eq. 2}$$

where the M-factor (*M*) stands for microstructure influence, and  $\sigma_{eff}$  and  $\sigma_0$  are the effective and intrinsic transport properties, respectively.<sup>35</sup> The M-factor includes the topological parameters, which are relevant for transport:

$$M = \frac{(\phi_P)^a \beta^b}{\tau^c} \qquad \qquad \text{Eq. 3}$$

Thereby,  $\phi$  is the volume fraction of the transporting phase. *P* is the percolation factor.  $\phi$  and *P* together combine into  $\phi_{\text{eff}}$ , which is the effective phase volume that contributes to transport. Constriction factor ( $\beta$ ) introduced by Petersen<sup>36</sup> can be interpreted as the ratio between the average sizes of the bottlenecks and the bulges  $(r_{min}^2/r_{max}^2)^2$ ,<sup>37</sup> and describes the bottleneck effect.<sup>38-40</sup> Tortuosity ( $\tau$ ) is a statistical expression for the windedness of transport pathways.<sup>41</sup> There are a few definitions of tortuosity. For example, the work with VMT<sup>34</sup> uses the so-called geometric tortuosity (with all transport pathways following a median axis skeleton), while another work of Stenzel *et al.*<sup>42</sup> uses geodesic tortuosity (with shortest transport pathways through the voxel-space of a given phase). The exponential parameters *a*, *b* and *c* are determined empirically with the above-mentioned VMT approach and with statistical error minimization. Following the work of Stenzel *et al.*<sup>42</sup> (where  $\tau$  represents geodesic tortuosity), the empirical relation in Eq. 3 takes the form:

$$M_{pred} = \frac{\phi_{eff} \beta^{0.36}}{\tau^{5.17}}$$
 Eq. 4

Whenever all the necessary topological parameters are known, the M-factor can be determined from Eq. 4 and the effective transport property from Eq. 2. One advantage of using such empirical relationships is the possibility to predict material properties that are difficult to access experimentally. For example in SOFC anodes, this approach opens new possibilities to gain information on the effective ionic conductivity in YSZ, which is usually not known or expensive to measure. More details on the methods to extract the required topological parameters from tomographic data can be found in previous works.<sup>37,43,44</sup> The topological parameters are also described in the experimental section below.

In the present study we use the above-mentioned methods to quantify topology and to predict effective transport properties in order to investigate microstructure effects of Ni-YSZ anodes. A special focus is laid on degradation mechanism upon redox cycling and on the redox stability. Ni-YSZ anodes of varying microstructure coarseness (fine, medium, coarse) before and after redox cycling at 950°C are investigated. The microstructures of fresh anodes and the corresponding electric and ionic conductivities are compared to each other. Then the influence of redox cycling on anode properties is documented in order to unravel the degradation mechanisms. We use the established empirical relationship between microstructure parameters and effective conductivity (resulting in  $M_{pred}$ ) and apply the predictive model to different SOFC anode microstructures. Also in this work, we determine the M-factor by numerical simulation of conduction ( $M_{sim}$ ), using the voxel-based tomography data as a structural input (with GeoDict software). The comparison of  $M_{sim}$  and  $M_{pred}$  can be considered as a validation of the empirical prediction approach.

So far the redox degradation was mainly described by qualitative observations (e.g. Ni agglomeration) or by measuring parameters, which cannot be linked directly to an effective property (e.g. average particle size). With the proposed approach where topological parameters are linked with conductivity on a quantitative level, the diagnosis of degradation effects becomes more specific. For example loss of conductivity can be directly related to change of bottleneck dimensions and associated constrictivity, or change of (average) length of transport pathway and associated geodesic tortuosity. As an outcome, the detailed analysis of microstructure parameters leads to a more differentiated interpretation of redox degradation. Finally, this knowledge leads to defining fabrication guidelines for

improved redox stability of Ni-YSZ anodes.

## 2. EXPERIMENTAL

The procedures for fabrication and electrical characterization of Ni-YSZ anodes are described in great detail by Iwanschitz *et al.*<sup>45,46</sup> The following sections (2.1 and 2.2) represent a short summary of the experimental procedures, followed by a description of the applied imaging and image analysis techniques (2.3 and 2.4).

#### 2.1. Anode fabrication and redox cycling

Three different anodes with fine, medium and coarse microstructures are produced by screen printing, oxidized sintering and subsequent reduction. To vary the microstructure three different powders (fine, medium, coarse) of 8YSZ (Mel Chemicals, purity > 99%) are mixed always with the same powder of NiO (J.T. Baker, purity > 99%) to form Terpineol-based slurries. The coarse powder is produced by calcination of the fine powder (Mel Chemicals). The ratio of the powders is chosen such that the solid volume fraction (Ni:YSZ) after reduction is 40:60. The Terpineol-based slurries are then screen-printed onto 3YSZ substrate (Nippon Shokubai, 140  $\mu$ m). The anodes are sintered in air at 1350°C for 4 hours after screen-printing. Subsequent reduction is performed at 950°C.

Degradation experiments are done by exposing the anodes to 8 redox cycles in a tube furnace at  $950^{\circ}$ C. For each cycle, reoxidation is carried out for 30 min and the re-reduction is carried out by ramping H<sub>2</sub> flow for 5 min, with equilibration time of at least 30 min.

#### 2.2. Electrical conductivity measurements

Four-point conductivity measurements are performed on 8.8 x 21 mm<sup>2</sup> samples cut from anode halfcells. The samples are placed in an alumina tube and contacted with Pt wire. The conductivity measurements are done at 950°C with a gas flow of 200 mL/min using forming gas (5% H<sub>2</sub>/95% N<sub>2</sub>). The Nernst potential is kept constant at 1.1 V during the measurements and the gas is not humidified in order to exclude ill-controlled degradation effects from water during the redox cycling. Between each redox cycle, the alumina tube is flushed with N<sub>2</sub> for 1 hour and the anodes are oxidized in airflow of 100 mL/min.

#### 2.3. Image acquisition by FIB-tomography and SEM

For microstructure analysis, polished cross-sections are prepared from the samples that were used for 4-point conductivity measurements. The porous anodes are first impregnated with a low-viscosity resin and then polished on textile substrates with 1, 3 and 6 µm diamond suspensions. Focused ion beam (FIB)-SEM tomography is performed with a Helios Nanolab 600i (FEI) with Ga liquid metal ion source.

FIB tomography includes a repetitive procedure of alternating ion sectioning and SEM imaging. The serial sectioning is done with an ion beam current of 2.5 nA and an accelerating voltage of 20 kV. For serial SEM imaging good contrast settings are achieved with the so-called through-the-lens detector (TLD) at 2.0 kV accelerating voltage and 0.69 nA beam current.

#### 2.4. Quantitative 3D microstructure analysis

FIB-tomography provides image stacks, which typically consist of 500 to 1000 2D images. Prior to the quantification of transport-relevant topological parameters the stacks have to be pre-processed. This procedure includes alignment (3D reconstruction), selecting a region of interest (cropping), noise filtering and segmentation (i.e. identifying Ni, YSZ and pore phases). In our workflow we use Fiji (<u>http://fiji.sc/Fiji</u>), including some home-made plug-ins and Avizo

(<u>http://www.fei.com/software/avizo3d/</u>) software packages. Further details on image processing can be found in our previous study.<sup>37</sup> 3D reconstructions of the fine, medium and coarse Ni-YSZ anodes before and after redox cycling are shown in Fig. 1. The corresponding dimensions of the tomographic data are summarized in the supplementary materials (Table S1).

Particle and pore size distributions are determined by a method called continuous phase size distribution (c-PSD), which was developed by Münch and Holzer.<sup>38</sup> Contrary to conventional PSD methods, which are based on a size statistics of discretized objects, c-PSD treats each phase as a continuum. A cumulative continuous size distribution is achieved by incrementally decreasing the size of spheres, which cover a particular phase volume and are completely contained in this volume. The radius corresponding to 50 vol% in the cumulative c-PSD curve ( $r_{50,max}$ ) is considered as a statistical measure for the average size of the phase. Hence, this so-called  $r_{50,max}$  represents the average size of bulges in a percolating network of either a solid or pore phase.

Based on 3D information from tomography mercury intrusion porosimetry (MIP), a method that describes pore size distributions by pressure infiltration can be simulated. According to the so-called Washburn equation,<sup>47</sup> the capillary radius is inversely proportional to the applied pressure. A cumulative MIP-PSD is thus obtained by linking the infiltrated volume with the corresponding pressure and capillary radius. It is well-accepted nowadays that the MIP-PSD mainly captures the size of bottlenecks, which dominate the infiltration process.<sup>48</sup> Here we apply the method of Münch,<sup>35</sup> which uses the same principle as for the c-PSD analysis. However, it adds the constraint that the incrementally added volume must be connected with the plane from where the infiltration starts. A cumulative MIP-PSD curve is thereby obtained by incrementally decreasing the sphere radius, which

corresponds to increasing pressures in the experimental MIP analysis. The 'inkbottle effect' governs the measurement like in the experimental counterpart, such that the dimensions of the bottlenecks limit the intrusion. Unlike the c-PSD, MIP-PSD measures the size of the bottlenecks ( $r_{50,min}$ ) once the breakthrough pressure is passed. Both methods can be applied to describe size distributions of pores as well as solid phases.

The constriction factor ( $\beta$ ) is given by the ratio of the cross-sectional areas of the bottlenecks to the bulges ( $A_{min}/A_{max}$ ) and further simplification leads to the following relation:

$$\beta = \left(\frac{\pi r_{min}^2}{\pi r_{max}^2}\right) = \left(\frac{r_{min}}{r_{max}}\right)^2 \qquad \qquad \text{Eq. 5}$$

This concept was adapted to describe bottleneck effects in disordered microstructures (e.g. fuel cell anodes).<sup>37</sup> For this purpose, the results from c-PSD ( $r_{50,max}$ ) and MIP-PSD ( $r_{50,min}$ ) are used to describe the average sizes of bulges and bottlenecks, respectively. By Eq. 5 we obtain the constriction factor ( $\beta$ ), which can be plugged into Eq. 4. Tubes of constant radius have a constriction factor of 1, while in disordered microstructures of varying radii the values are <1.

Geodesic tortuosity,  $\tau_{geod}$  (simply  $\tau$ ) is defined as the ratio of geodesic distance ( $d_{geod}$ ) and material thickness (*l*). In general, the geodesic distance can be interpreted as the shortest path length from one side of the material to the other side through the transporting material phase. For statistical accuracy, we consider the mean value of geodesic distances (shortest path lengths) for numerous starting points. More precisely, any pixel in the so-called in-plane, which belongs to the transporting phase, is considered as starting point for shortest path analysis. The shortest path lengths are calculated using Dijkstras algorithm.<sup>49</sup> Therefore, the image is interpreted as a graph in which each voxel of the transporting phase is a node and all the nodes are connected whenever the corresponding voxels are connected with respect to the 26-neignborhood. Note: The geodesic tortuosity should not be mixed up with the geometric tortuosity. For the latter Dijkstras algorithm is applied to a skeleton graph of the transporting phase. The two methods were compared in a recent study by Stenzel *et al.*<sup>42</sup> and concluded that the geometric definition overestimates the tortuosity, while the geodesic definition captures tortuosity with respect to the conductive transport processes more adequately.

#### 2.5. Conductivities and M-factors simulation

Equations 2-4 describe a method to predict effective conductivities by using quantitative microstructure analysis and M-factor ( $M_{pred}$ ), respectively (see Eq. 4). As an alternative approach, the effective ionic and electrical conductivities are also assessed by numerical simulation using the

software GeoDict (http://www.geodict.com/). The mathematics involved in the simulation is extensively described by Wiegmann and Zemitis.<sup>50</sup> The simulations of electrical and ionic conductivities were done along x, y and z directions using the real tomographic data as input. It should be noted, that for the case where the phase of interest takes an intrinsic conductivity value of 1, (while all other phases are set to 0), the obtained conductivities also represent the M-factor (i.e.  $M_{sim}$ ). The results from simulation ( $M_{sim}$ ) are subsequently compared to the results from the predicted M-factor from microstructure analysis ( $M_{pred}$ ). The dimensions of the tomographic 3D data used in the simulations are summarized in Table S2 in the supplementary materials.

#### 3. RESULTS

#### 3.1. Qualitative description of microstructures

The initial microstructures are strongly influenced by the sintering process and the initial reduction conditions. It is important to note that the morphological characteristics of Ni and pores are influenced by the coarseness of the YSZ powder. During the anode fabrication only the starting particle size of the YSZ powder is varied (fine, medium, coarse) while the particle size of NiO is the same for all the samples.

The visual inspection of 3D reconstructed images in Fig. 1 and 2D segmented images in Fig. 2 show that upon sintering and reduction the microstructures of Ni and pores are adapting to the microstructure of YSZ. This adaptation already starts during sintering in air (before reduction), where NiO changes its size according to the coarseness of YSZ (not shown here). Hence the anodes fabricated with coarser YSZ also exhibit coarser microstructures of Ni and pore phases. However, the inspection of 3D images also indicates that Ni and YSZ have different characteristics. YSZ appears to be more granular with distinct sinter necks, whereas Ni forms a more continuous network with a greater structural heterogeneity.

The microstructure degradation related to redox cycling can be observed in Fig. 2 by comparing top (before) and bottom rows (after redox). Significant Ni coarsening is observed after redox cycling. Ni tends to form agglomerated patches, which is particularly strong in the fine anode. In contrast, the microstructure of YSZ seems to withstand redox alterations. This is compatible with the interpretation of YSZ being the rigid backbone of Ni-based anodes. An additional aspect of redox degradation is the increase of inter-granular porosity, which is again stronger in the fine anode. On a macroscopic scale the increase of pore volume fraction may result in an overall swelling. Consequently, the swelling will invoke a relative decrease of the solid volume fractions.

#### 3.2. Electrical conductivity measurements

Figure 3 shows the evolution of electrical conductivities ( $\sigma_{eff}$ ) during 8 redox cycles at 950°C.<sup>45</sup> The fine sample exhibits the greatest degradation of  $\sigma_{eff}$ , while the coarse sample even shows an improvement in  $\sigma_{eff}$ . Significant differences are measured for the initial values (0<sup>th</sup>) and for the 1<sup>st</sup> redox cycle. These initial differences are not well understood. They may be related to experimental issues such as contacting and/or to microstructure reorganization after reduction. In contrast the linear trends from 1<sup>st</sup> to 8<sup>th</sup> cycle are interpreted as typical redox behavior. Therefore in the discussion, the values of  $\sigma_{eff}$  after the 1<sup>st</sup> redox cycle are taken as the reference electrical conductivity ( $\sigma_{eff,before}$ ). The last redox cycle (8<sup>th</sup>) is taken as the electrical conductivity after redox cycling ( $\sigma_{eff,after}$ ). The data set in Fig. 3 will be compared to predicted transport properties, which are based on topological parameters obtained from 3D image analysis (see Eqs. 3 and 4).

#### 3.3. Effective volume fractions ( $\phi_{eff}$ , $\varepsilon_{eff}$ ) and percolation (P)

In the subsequent sections (3.3 -3.5) we present results from quantitative 3D analysis, with a strong focus on parameters that are relevant for the effective transport properties. The porosities ( $\varepsilon_{eff}$ ) of the six investigated SOFC anodes are shown in Fig. 4, and the ratios of solid volume fractions ( $\phi_{Ni}/\phi_{YSZ}$ ) are presented in Fig. 5. Before exposure to redox cycling, the porosity increases from fine (25 vol%) over medium (36%) to coarse (39%). During redox cycling, the porosity increases in all three microstructures, which is most pronounced in the sample with the fine microstructure (83 % increase) compared to medium and coarse samples (8 and 12%).

The ratios  $\phi_{Ni}/\phi_{YSZ}$  are similar for all six samples before and after redox cycling (40:60 vol%) as shown in Fig. 5B. However, considerable differences occur with respect to the effective volume fraction ( $\phi_{eff}$ ), which is defined as the product of the total volume fraction ( $\phi$ ) multiplied by the percolation factor (*P*). The latter parameter describes the fraction of a phase, which forms a connected network, and it can be obtained from an MIP-PSD analysis of 3D images previously mentioned (Fig. 5A). Before exposure to redox-cycling the percolation factors are close to 1. The cumulated percolation factors for Ni, YSZ and pores together comprise 0.991, 0.985 and 0.962 in fine, medium and coarse microstructures, respectively. After redox cycling, the percolation factors of YSZ and Ni decrease. This change is particularly strong for YSZ in the coarse sample, where the percolation factor drops to 0.18. For the Ni phase the changes are largest in the fine sample, where the *P* drops from 0.99 to 0.80 (compared to 0.90 in coarse). In all samples the *P* of pores remains close to 1 before and after redox cycling. 3.4. Phase size distributions (PSD), average radii ( $r_{50,max}$ ,  $r_{50,min}$ ) and constriction factor ( $\beta$ ) The c-PSD and MIP-PSD curves for Ni in fine and coarse anodes are shown in the supplementary materials (Fig. S1). The PSDs for medium-grained anodes are not shown for simplicity. The average radii ( $r_{50,max}$ ,  $r_{50,min}$ ) and associated constriction factors of Ni are summarized in Fig. 6. The  $r_{50,max}$  of Ni particles in fine, medium and coarse anodes are 378, 540 and 636 nm (Fig. 6a) and the average bottleneck sizes ( $r_{50,min}$ ) are 204, 275 and 300 nm (Fig. 6b). Although the bulges and bottlenecks increase from fine to coarse, the constriction factor ( $\beta_{Ni}$ ) exhibits a slightly decreasing trend from 0.29 (fine) to 0.22 (coarse) (Fig. 6c).

Upon redox cycling the c-PSD curve for Ni in the fine anode is shifted to the right after redox cycling (Fig. S1A). The average size of Ni ( $r_{50,max}$ ) increases from 378 nm (before) to 517 nm (after redox) (Fig. 6a). For medium and coarse microstructures, the c-PSDs and associated average Ni size ( $r_{50,max}$ ) remain almost unchanged. In contrast, the Ni bottlenecks ( $r_{50,min}$ ) in all the samples exhibit an increase upon redox cycling with the most significant change for coarse anodes (Fig. 6b). Consequently, in the fine sample the constriction factor ( $\beta_{Ni}$ ) decreases significantly from 0.29 to 0.18 (Fig. 6c) mainly due to grain growth (increase of  $r_{50,max}$ ). In the medium and coarse samples  $\beta_{Ni}$  increases to 0.34 and 0.37 due to opening of bottlenecks (Fig. S1B, increase of  $r_{50,min}$ ) after redox exposure.

As illustrated in Fig. 7a, the YSZ phase exhibits increasing size of the bulges from fine to coarse before redox cycling. The initial average radii of the bulges are 360, 557, and 981 nm for the fine, medium and coarse samples, respectively. This is accompanied by decreasing average radii of the bottlenecks (195, 172, and 82 nm, Fig. 7b). Consequently, the constriction factor ( $\beta_{YSZ}$ ) before redox cycling decreases from 0.37 to 0.007 (fine to coarse). The ceramic phase is usually described as a rigid backbone in the composite anodes, which resists mechanical stress and morphological degradation. Nevertheless, for samples with a coarse microstructure a significant decrease of 25% in the size of bulges is observed upon redox cycling (Fig. 7a). In the fine and medium samples the changes in the size of the bulges ( $r_{50,max}$ ) are small (+6% for fine and -4% for medium). In YSZ the bottleneck radii change considerably upon redox cycling. For example in the coarse sample the initially small bottleneck radius ( $r_{50,min}$ ) decreases again by 90%. But also in fine and medium samples the neck radii decrease strongly (Fig. 7b).

The average sizes of bulges and bottlenecks in the porous network, as well as the corresponding constriction factors are shown in Fig. 8. The size of the bulges and the bottlenecks of the pores increase as the initial microstructures become coarser. The biggest change in the pore structure upon

redox cycling concerns the increase of the bottleneck radius in fine anodes (Fig. 8b), which may be related to the qualitatively observed swelling. Before redox cycling, the constriction factor ( $\beta_{Pore}$ ) in the fine sample is relatively low (0.25), compared to medium and coarse. After redox cycling the  $\beta_{Pore}$  is relatively large (0.5 ± 0.1) in all three samples.

#### 3.5. Geodesic tortuosities, $(\tau)$

The geodesic tortuosities of Ni, YSZ and pores are shown in Fig. 9. In general, the geodesic tortuosities vary only in a narrow range between 1.0 and 1.5. Exceptionally high tortuosities are observed in the coarse samples for Ni (1.7 before and 1.6 after redox) and for YSZ (before redox). Before redox cycling, the tortuosities of Ni and YSZ tend to increase from fine to coarse (Figs. 9a and 9b). Upon redox cycling, the tortuosities of Ni and YSZ tend to increase in all samples except for YSZ in the coarse anode. However, the results for YSZ of the coarse sample must be questioned, because the representative elementary volume (REV) may be larger than the image window. The REV for coarse YSZ is very large, due to the significant loss of percolation upon redox cycling (see also Fig. 5). In the initial state, the tortuosities in the pore structures (Fig. 9c) increase from coarse to fine samples, which may be attributed to stronger densification of the fine anode upon sintering. After redox cycling, the tortuosities in the pores are generally low, which is due to the macroscopic swelling and associated opening of the pore networks.

3.6. Simulation of effective transport properties ( $\sigma_{eff}$ ) and microstructure factors ( $M_{sim}$ )

Effective conductivities and the corresponding microstructure factors ( $M_{sim}$ ) can be assessed by means of numerical simulations. In order to capture the microstructure effects in a realistic way, 3D information from tomography is used as geometric input. In this study the transport simulations are performed with the commercial software GeoDict.

As shown in Fig. 10b, the M-factors ( $M_{sim}$ ) of YSZ in the fresh samples tend to decrease from fine to coarse. Hence, fine microstructures appear to be preferable. However, the M-factors of YSZ decrease strongly upon redox cycling, which leads to strong limitations for ionic conductivities. In the coarse microstructure this limitation is already present in the initial microstructure (before redox) due to the low sintering activity and strong constrictions at the bottlenecks.

The trends observed for ionic conductivity in the simulation (i.e. decreasing M-factors from fine to coarse) are caused mainly by the reduction of bottleneck radii for coarser microstructures and by the associated reduction of constriction factors. These variations can be attributed to the inverse relationship between particle size of YSZ and the corresponding sintering activities (i.e. coarser YSZ

tends to have smaller). Apparently, in the coarse sample the necks are so weak, that mechanical stresses from redox cycling even lead to a loss of connectivity between the YSZ particles (see Fig. 5: drop of percolation factor) and to a reduction of the effective volume fraction. In the fine sample there is also an increase of tortuosity, which contributes to the significant reduction of the M-factor during redox cycling.

The M-factors ( $M_{sim}$ ) of Ni vary in a relatively narrow range between 0.01 and 0.08. Before redox cycling, the M-factors of Ni decrease from fine to coarse. This result implies that in the fresh anode, fine microstructures are preferred due to the relatively high initial effective electrical conductivity. After redox cycling, the M-factor of Ni in fine sample decreases, while the M-factors of medium and coarse increase. Overall, the simulated effective electrical conductivities in all investigated anodes are still relatively high even after redox cycling, since they reach 1 to 8% of the intrinsic conductivity in bulk nickel. As mentioned above, since transport distances in thin anode layers are short, these effective electrical conductivities are not expected to impose significant limitations to the anode performance. However, as discussed later, the results for nickel in the medium and coarse microstructure have to be interpreted carefully, because the corresponding REV is very large, possibly even exceeding the thickness of the anode layer.

# 4. DISCUSSIONS

This study focuses on three main points: (1) Evaluation of the possibility to predict anode conductivities based on an empirical relation (Eq. 4) between the measured topological parameters and effective transport properties. The empirical equation was developed by means of virtual materials testing (i.e. analyzing virtual microstructures from a stochastic model). In this first part, the aim is to test whether this relationship also holds for real microstructures (i.e. porous Ni-YSZ anodes). (2) Understanding redox degradation mechanisms in Ni-YSZ anodes, with a special focus on effective transport properties. The knowledge of micro-macro relationships (Eq. 4) enables to determine specific contributions to the degradation of conductivities, which originate from quantifiable changes of specific, transport-relevant topological parameters. This level of detail is novel and potentially sheds new light on degradation mechanisms. (3) Formulate fabrication guidelines and design concept for improved redox-stable Ni-YSZ anodes. The mechanisms and degree of degradation are related to the initial microstructure (fine, medium, coarse). These information can be used to test new concepts for redox stable anode microstructures with high electrical and ionic conductivities, which may be obtained by mixing powders with different fineness.

#### 4.1 Prediction of effective transport properties

In the results section, we have presented topological parameters that are relevant for transport properties. In addition, the effective electrical and ionic conductivities were determined by numerical simulation ( $M_{sim}$ ) using 3D microstructures as input. At this point, we intend to predict the effective electrical conductivity based on the topological parameters using Eq. 4. A plug-in of the topological parameters ( $\phi_{eff}$ ,  $\beta$ ,  $\tau$ ) obtained from 3D microstructure analysis into this equation gives the predicted M-factors ( $M_{pred}$ ). A summary of the topological parameters for Ni and YSZ, as well as the predicted Mfactors from Eq. 4 is listed in Table S3 in the supplementary materials. As shown in Fig. 11,  $M_{pred}$  of Ni and YSZ before redox cycling follows the same trends as  $M_{sim}$  (Fig. 10). The trends show highest effective conductivities for the fine anode, which decrease to the coarse anode. Figures 11c and 11d also present the specific contributions of each topological parameter weighted by the exponents from the empirical Eq. 4 (i.e.  $\phi_{eff}$ ,  $\beta^{0.36}$ ,  $\tau^{-5.17}$ ) and normalized against the values of the fine anode. The decrease of  $M_{pred}$  for Ni from fine to coarse is highly influenced by changes of tortuosity and effective volume fraction, while the decrease of  $M_{pred}$  for YSZ is related to variations in constrictivity and tortuosity. The variation of constrictivity in YSZ is compatible with particle-size dependent sintering activity, which was discussed earlier (see Fig. 7).

The correlations between  $M_{\text{pred}}$  and  $M_{\text{sim}}$  are shown in Fig. 12. Before redox cycling a strong correlation between  $M_{\text{pred}}$  and  $M_{\text{sim}}$  is observed (Figs. 12a, 12b). This is a clear indication that the empirical relationship in Eq. 4 is indeed able to predict the effective transport properties of real microstructures. However, for samples after redox cycling (Figs. 12c, 12d) the correlation plot shows a more complex pattern. A good correlation between  $M_{\text{pred}}$  and  $M_{\text{sim}}$  is only obtained after redox cycling for YSZ (Fig. 12d). However for Ni, it is only for the fine anode as shown in Fig. 12c. The data points of medium and coarse anodes plot at some distance away from the reference line. The reason for this mismatch is not clear. However, it can be suspected that it may be related to greater heterogeneity in the microstructure, which leads to larger REV as it is shown in the following. If the REV becomes similar in size or larger than the sample, our analysis becomes flawed, which is suspected to be the case of the medium and coarse microstructure after redox cycling.

The different degrees of heterogeneity and associated potential problems with the size of the REV are illustrated in Figs. 13 (fine anode) and 14 (medium and coarse). The figures show fluctuations of two topological parameters profiles through the anode layers. Figures 13a, 13b, 14a, and 14b represent the effective volume fractions from stacked 2D analysis, whereby for each 2D image (y-z plane) a

connectivity check is performed with the inlet plane on the left (x-direction). If connectivity with the left side is lost completely, then the effective volume fraction drops to 0. Minor fluctuations of the volume fractions may arise when the size of 2D slices is not fully representative. Figures 13c, 13d, 14c, and 14d show the fluctuations in tortuosity. Here each value at a specific distance (*x*) includes a complete 3D analysis (i.e. transport pathways from location *x* to the inlet plane are measured). Close to the inlet plane the pathways typically have straight connections, which results in tortuosity values close to 1. A plateau value is reached at larger distances, when the thickness is large enough to include a representative volume. The effective volume fractions of Ni and YSZ in the fine anode vary only in a limited range (Figs. 13a, 13b). This indicates that connectivity issues are not important for this sample and even the single 2D images ( $15 \times 25 \mu m^2$ ) have (almost) a representative size. After redox the solid volume fractions are lower, because of macroscopic swelling and increase of porosity.

The tortuosities of Ni and YSZ (fine, before redox) approach plateau values, which again confirms that the 3D volume has a representative size (Figs. 13c, 13d). After redox cycling the tortuosities are much higher and especially for Ni the fluctuations increase considerably, which indicates that the thickness of the 3D volume is at a lower limit for being representative. In summary the results in Fig. 13 indicate that the analyses of fine anodes are reliable (i.e. representative), which is also confirmed by the good correlations in Figs. 12a and 12b.

For the medium and coarse anode the fluctuations of volume fractions are higher (Figs. 14a, 14b). In particular for coarse YSZ after redox cycling the effective volume fraction drops to 0 at a distance of *ca*. 7  $\mu$ m, which is attributed to a loss of connectivity. However, the apparently complete loss of connectivity might be related to a limited size of the image window. Potentially some connected pathways may exist outside the image window. For tortuosity (coarse anode) the fluctuations are even higher. The curve for YSZ also ends at a distance of *ca*. 7  $\mu$ m, which is again due to loss of connectivity (Fig. 14d). Overall, the coarse anode has a much larger REV that is not always captured in the image windows. Especially for the coarse anode after redox cycling the size of the tomographic data is smaller than the REV, which may explain the mismatch between  $M_{pred}$  and  $M_{sim}$  in the correlation plot (Figs. 12c, 12d). Similar problems are identified for the medium-grained anode after redox cycling.

In the context of concerns over the REV size, it must be emphasized that computational limitations are generally higher for numerical simulation compared to the ones for topology analysis. Due to the limitation in memory and computing time, smaller sub-volumes are used as a structural input for

numerical simulation with GeoDict. Figure 15 represents a correlation plot of the medium-grained anode, which highlights the problems related to different image window sizes used for simulation and image analysis. Before redox cycling a reasonable correlation is obtained between M<sub>sim</sub> and M<sub>ored</sub> (data point marked with filled triangle), although the simulation is performed on the basis of a smaller 3D image window. Hence, even with the smaller image window a representative analysis is obtained for pristine anodes. Upon redox cycling the heterogeneity increases and thus the REV becomes larger. The corresponding data point represented by an open triangle (Fig. 15 left) is far away from the reference line. In this case the topology analysis is based on a larger image window (marked with 'A' in Fig. 15 right) compared to the one for numerical simulation (marked with 'B'). The size dependence indicates that at least with the smaller window 'B' the REV is not reached. If both analyses are based on the same image window, then the correlation is still good (see data point marked with a star in Fig. 15 left). Hence, even if the image window is below REV (as it is in this case), a good correlation can be achieved. This finding can be considered as an additional confirmation that the empirical relationship (Eq. 4) is capable to reliably predict the effective transport properties. On the other side, it must be noted that throughout this study numerical simulations are performed on smaller image windows than the corresponding topology analyses. Good correlations of  $M_{sim}$  and  $M_{pred}$  (e.g. for all anodes before redox cycling) thus indicate that these analyses are based on a representative image window.

#### 4.2 Degradation mechanism

Effective conductivities from simulation ( $M_{sim}$ ) and from image analysis ( $M_{pred}$ ) show a good correlation, provided REV is not too large with respect to the sampled image size. This is interpreted as a positive validation of the underlying empirical relationship (Eq. 4). However, both, simulation and image analysis basically use the same type of data from tomography as input. A thorough validation should therefore rather be based on independent measurements. Hence, the experimental electrical conductivities presented in Fig. 3 can be used for this.

Fig. 16 shows a comparison of experimental data (open symbols) and  $M_{pred}$  from image analysis (filled symbols), and how these properties degrade upon redox cycling. The experimental data are presented as relative conductivity, whereby for each data series the measured electrical conductivity after *n* redox cycles is normalized by the measured conductivity after the 1<sup>st</sup> redox cycle for the considered series. As discussed earlier, the experimental data (Fig. 3) shows linear trends between the 1<sup>st</sup> to 8<sup>th</sup> redox cycles, which is interpreted as a result from microstructure degradation. However, the initial

values and the degradation during the 1<sup>st</sup> cycle also show strong irregularities for the three different anodes, which is speculated to result from experimental artifacts. The influence of these uncertainties can be suppressed by taking the value after the 1<sup>st</sup> cycle (instead of 0<sup>th</sup>) as a basis for normalization. Normalized M-factors are based on tomographs from anodes after the 0<sup>th</sup> and 8<sup>th</sup> cycle. In the tomographic data, the 3D microstructure after the 1<sup>st</sup> cycle was not obtained. Nonetheless, the comparison shows that the trends for degradation upon redox cycling are very similar for experimental conductivities as for the predicted M-factors. In both cases, the fine anodes show a high degradation rate, whereas degradation rates in the medium- and coarse-grained anodes are very low. For the coarse anode the experimental measurements even indicate a positive effect of redox cycling (i.e. increasing conductivities after redox exposure). In summary, the experimental results support the validity of the suggested empirical relationship (Eq. 4) to predict effective conductivity. Even though for some samples (e.g. coarse, after redox) the image size of tomographs is at the lower REV limit, there is still a good correlation between predicted and experimentally measured degradation rates. In the following section the modes of degradation after redox cycling are discussed separately for the fine and coarse samples. In Figs. 17 and 18 the normalized M-factors and normalized topological parameters are used in order to illustrate details of microstructure degradation. Normalization in this case means plotting the ratios of values obtained after 8 redox cycles over the values from pristine samples. The ratio of the microstructural parameter is elevated to the same power as in Eq. 4, so that this ratio directly reflects the impact on the M-factor change.

This reveals that in the fine sample, degradation of the normalized M-factor of Ni is mainly due to changes of tortuosity and volume fraction. This is compatible with results in Figs. 4 and 9 where a significant decrease in connectivity (effective volume fraction) and increase in tortuosity are observed in the fine sample. For YSZ, the normalized M-factor of only 0.1 indicates a strong degradation. This is caused by significant changes in tortuosity, and to a lower degree by changes in constrictivity. It is important to note that Ni agglomeration is a very evident feature in all Ni-based anodes. However, with respect to the degradation of effective transport properties, our results for the fine anode indicate that the degradation rates are higher for YSZ (i.e. ionic conductivity) than for Ni (i.e. electrical conductivity). This is surprising, considering that a relatively high sintering activity in fine microstructures leads to relatively strong bottlenecks of YSZ. This example thus also illustrates that detailed quantitative analysis can provide counter-intuitive results, which contradict widespread interpretations of Ni agglomeration that are mainly based on qualitative observations that suffer from lack of microstructural

characterization and quantification.

For the coarse sample the influence of the topological parameters on the degradation of *M*<sub>pred</sub> in Ni is shown in Fig. 18. In general, the transport properties of Ni do not degrade during the 8 redox cycles, because the influence of a worsened tortuosity is compensated by improved constrictivity (i.e. wider bottlenecks). In addition, unlike for the fine anode, redox cycling did not involve remarkable loss of connectivity in the fine Ni network. For YSZ in coarse anodes the redox cycling leads to significant degradation of the M-factor and associated ionic conductivity. This is attributed to substantial loss of connectivity (see Fig. 5, and discussion of size-dependent sintering activity). This loss of connectivity also leads to larger REV, which questions the reliability of the corresponding topological analyses of coarse YSZ after redox cycling.

Our interpretation of microstructural results leads to the postulation of different modes of Ni growth, depending on the coarseness of the initial microstructure. These modes are qualitatively illustrated in Fig. 19. For the fine sample, Ni coarsening happens mainly along the bulges of the Ni network (indicated as red domains in Fig. 19a). It is suggested that the smallest Ni particles from the initial microstructure have a relatively high mobility, due to a high surface energy. Preferably the mobile Ni becomes enriched at the pre-existing bulges in the Ni network and/or they may also form new isolated islands. This is also supported by the results for the fine anode in Fig. 6, which show that the size of the Ni bulges ( $r_{50,max}$ ) increases during redox cycling and the connectivity of Ni decreases at the same time. In addition, in the fine microstructure also YSZ and pores both form fine-structured networks, which leave not much space for unconstrained Ni coarsening. As a consequence, the reorganization of Ni also induces strain in the YSZ phase, which is localized along the bottlenecks. This also leads to lower constrictivity in YSZ and to lower ionic conductivity.

For coarse anode microstructures, the Ni growth is mainly localized along the bottlenecks (as indicated by red domains in Fig. 19b). As shown in Fig. 6 for coarser samples, the increase in constrictivity is mainly caused by an increase in bottleneck sizes. These results explain why the electric conductivity and associated M-factors for Ni are more stable in coarse than in fine anodes. According to experimental results redox cycling may even lead to higher electric conductivities, which may be attributed to the widening of bottlenecks.

While Ni coarsening is an obvious feature of redox degradation, YSZ is also affected by the stress associated with the Ni agglomeration. For example, Fig. 20 shows the splitting of YSZ particles invoked by the Ni growth. The strain is most probably concentrated along the sinter necks, which is

weakest for the coarse anode. Consequently, the YSZ disintegrates and loses percolation. In summary, the different modes of Ni agglomeration can be explained by the fact, that the fine microstructure has a granular texture with numerous fine particles. Reduction of surface energy is achieved when Ni is redistributed from small particles to larger ones. In contrast, in the coarse microstructure Ni forms a more continuous network with a sinusoidal surface morphology. The surface energy is minimized when mobile Ni moves into the concavities (i.e. bottlenecks).

#### 4.3. Mixing different powders

The optimization of redox stability of Ni-YSZ has also been investigated by using various techniques such as addition of Mg species,<sup>51</sup> infiltration of a polymeric NiO precursor into the YSZ skeleton,<sup>52</sup> dispersing fine YSZ particles on the surface of NiO,<sup>53</sup> and lowering of reoxidation temperature.<sup>54</sup> Based on the knowledge gained in this study we suggest addressing the issue of redox degradation by combining the advantages of different microstructure fineness (see Table 1). According to this study, the fine anode has the highest initial electrical and ionic conductivities. Moreover, it has the advantage of strong YSZ bottlenecks, which ensures relatively stable ionic conductivity (and supposedly high TPB). However, in terms of redox stability, the anode with coarse microstructure has distinct advantages, mainly because it has a higher initial porosity, which leaves more space for the volume expansion upon oxidation. In the coarse anode Ni undergoes low loss of percolation and mobilization of Ni even leads to wider bottlenecks, which has a positive effect on electric conductivity. The disadvantage here is the relatively low sintering activity of YSZ. Consequently, for improved redox stability we combine 50:50 vol% ratio of fine and coarse, as well as fine and medium powders of YSZ. This should lead to higher initial conductivities (from fine), but increase the redox stability of Ni (coarser pores) and of YSZ (fine particles as sinter help).

The relative electrical conductivities (Fig. 21) show that in 50:50 mixtures the degradation behavior is mainly dominated by the properties of the fine powder and microstructure. The addition of medium and coarse powders seem to lower the degradation rate of the electrical conductivity but obviously the 50% fine is too high. For further optimization we thus suggest to lower the amount of the fine powder (e.g. 10%). Such anode compositions should have better resistance to both ionic and electrical conductivity degradation.

It must be emphasized that in this study we focused on the effective transport properties. A strong limitation thereby is the lack of experimental measurements for ionic conductivity. Since the intrinsic conductivity of YSZ is much lower than the one of Ni, it follows that with respect to anode performance

the effective ionic conductivity is also more limiting than the electronic conductivity.<sup>55</sup> These investigations show that degradation of YSZ (i.e. reduction of M-factor) during the redox cycling can be even worse than the degradation of Ni. Significant loss of connectivity is observed for coarse YSZ, which hinders distribution of ions throughout the anode layer. In principle the properties of an anode do not have to be constant over the entire thickness. The functional layer close to the anodeelectrolyte interface should have high electrochemical activity (TPB length) and high ionic conductivity. The anode regions at larger distances away from this interface rather serve as current collector and hence they should have high electric conductivity. This leads to the well-known concept of doublelayered anodes.<sup>20,24,25</sup> A fine-grained anode is used as the functional layer (e.g. with 60 vol% YSZ vs. 40vol% Ni) and the coarse grained material is suitable to serve as a current collector (e.g. with 50 vol% YSZ vs. 50 vol% Ni). In this context, addition of small amounts of fine YSZ (e.g. 5 vol%) to a generally coarse anode microstructure may lead to a current collector with stronger bottlenecks. However this latter hypothesis has not yet been tested.

#### 3. CONCLUSIONS

In this study we investigate the relationship between microstructure and effective transport properties in Ni-YSZ anodes and the corresponding degradation upon redox cycling. Our microstructure investigations reveal a complex pattern of different materials properties and degradation behaviors, which vary depending on the coarseness of the initial microstructure.

- Comparison of fine vs. coarse anodes - before redox cycling

In the initial state the fine anode has higher electrical and ionic conductivities compared to the coarse anode. The M-factors predicted from topology analysis and from numerical simulation are consistent with each other. These M-factors decrease from fine to coarse microstructures for both phases (Ni and YSZ). For Ni, the lower M-factor in the coarse anode is mainly related to a higher tortuosity and a lower effective volume fraction (due to low connectivity). For YSZ, the lower M-factor in the coarse anode can be attributed to a higher tortuosity and a lower constrictivity (small bottlenecks, low sinter activity).

#### - Comparison of Ni in fine vs. coarse anodes - after 8 redox cycles

Upon redox cycling at 950°C, Ni coarsening and YSZ loss of percolation are the most obvious features of anode degradation but the degree of degradation strongly depends on the initial particle size and on the fineness of the microstructure. The fine anode is affected by substantial Ni coarsening, which leads to a significant loss of percolation and increase of tortuosity. This microstructure degradation is

compatible with the experimentally measured drop of electrical conductivity by *ca*. 50% over 8 redox cycles. In the coarse microstructure Ni-coarsening is also a prominent feature, however due to larger pores, the spatial rearrangement of Ni is less harmful than in the fine anode. In the coarse anode loss of percolation as well as changes of tortuosity and constrictivity are relatively small. Moreover, this microstructure degradation is compatible with the experimental data showing a stable evolution of the electrical conductivity over 8 redox cycles.

#### - Comparison of YSZ in fine vs. coarse anodes - after 8 redox cycles

Redox cycling and associated re-arrangement of Ni exerts stresses onto the rigid YSZ structure. In the fine sample, YSZ has stronger necks due to a higher sintering activity. Consequently the fine YSZ remains relatively stable upon redox cycling. In contrast, the coarse YSZ has a lower mechanical stability due to weaker sinter necks. In coarse anodes redox cycling leads to significant loss of connectivity between the large YSZ grains, despite the fact that the pores are more open and Ni has more room for volume expansion upon oxidation. The loss of connectivity also induces a strong increase of tortuosity. Together with a decrease in constrictivity, these three degradation phenomena (i.e. changes of *P*,  $\tau$ ,  $\beta$ ) lead to a significant drop of the YSZ M-factor and of the corresponding ionic conductivity in the coarse anode.

Also in this study, we followed a hypothesis that a mixture of fine- and coarse- (or medium-)grained particles would be beneficial to slow down degradation of both phases (Ni and YSZ) and associated drop of conductivities. First experimental results in this direction indicate that mixtures with 50% fine and 50% coarse YSZ powders are not ideal. In the 50:50 (fine:coarse) mixtures the Ni coarsening and YSZ degradation appears to be dominated by the negative properties of fine particles and pores. Consequently it is suggested that a smaller amount of fine YSZ may be sufficient to increase the stability of the sinter necks between larger YSZ particles. This improvement is important since, in general, ionic conductivity is a strongly limiting factor for high anode performances (i.e. distribution of  $O^{2^{2}}$  ions within the anode). In addition, relatively coarse pores are considered to be beneficial in the sense that they represent buffer space during the expansion upon Ni oxidation to NiO, which is not available in the fine-grained anodes due to higher density after sintering. The coarser pores may be introduced also with suitable pore formers. In conclusion, for future improvements of anode performance and redox stability we propose a mixture of (<50%) fine and (>50%) coarse YSZ powders and the addition of relatively coarse pore formers. The optimum proportions of these components are yet to be defined.

Aside from the insights mentioned above, the following conclusions can be drawn with respect to the suitability of methods to study microstructure effects. In this study, the relationship between conductivity and microstructure was investigated in two ways: (1) by numerical simulation of conductivity and (2) by using an empirical relationship that allows prediction of effective conductivities based on topological parameters from 3D analysis. With respect to numerical simulation it is important to note that in the past conventional FE-Analysis was strongly limited by the number of structural elements (grid points). Therefore it was necessary to transform the high-resolution tomographic data (voxels) into lower resolution meshes (cubic or tetragonal). However, recent progress of commercial simulation tools (e.g. GeoDict, Avizo) allows running simulations on voxel grids >5003 in a reasonable time. The option to perform computations directly on the voxel grid from tomography represents a considerable improvement. For the initial anode microstructures investigated in this study, this size is sufficient to describe as REV at a resolution that is high enough to capture the relevant details (e.g. small bottlenecks and connectivity). However, after redox cycling the representative volume is clearly larger and the results obtained from numerical simulation are not reliable. The second method (i.e. topological analysis) can handle larger data volumes and the limitations regarding REV are less severe. Nevertheless, for the coarse anode after redox cycling the structures are very heterogeneous and the REV is strongly enlarged. This size could not be reached with either of the methods. For this reason, the results for coarse anodes after redox cycling must be considered as qualitative and preliminary.

A further methodic aspect is the fact that transport simulations do not provide the specific topological parameters, which control the anode performance. 3D imaging and topological analyses are necessary to capture the complex picture of microstructure degradation and its relation with effective properties. In summary, since both methods provide complementary information, a combination of the two methods is considered as being ideal to study such microstructure effects.

#### Acknowledgments

The financial support of the Swiss National Science Foundation (contract 200021-135270) is gratefully acknowledged. The authors are also thankful for the support of the Scientific Center for Optical and Electron Microscopy (ScopeM) of the ETH Zurich. We also would like to thank G. Peschke (IfB, ETH Zurich), Dr. J. Reuteler (ScopeM), and Dr. B. Münch (EMPA) for the assistance and technical support.

# REFERENCES

- L. J. Gauckler, D. Beckel, B. E. Buergler, E. Jud, U. P. Muecke, M. Prestat, J. L. M. Rupp, and J. Richter, "Solid Oxide Fuel Cells: Systems and Materials," *Chimia*, **58** [12] 837-850 (2004).
- 2. J. Mantzaras et al., "Fuel Cell Modeling and Simulations," Chimia 58 [12] 857-868 (2004).
- S. B. Adler and W. G. Bessler, "Elementary kinetic modeling of solid oxide fuel cell electrode reactions"; pp. 441-462 in *Handbook of Fuel Cells – Fundamentals, Technology and Applications, Vol. 5.* Edited by W. Vielstich, H. Yokokawa, and H.A. Gasteiger. John Wiley & Sons, Chichester, UK, 2009.
- O. Pecho, L. Holzer, Z. Yáng, J. Martynczuk, T. Hocker, R. J. Flatt, and M. Prestat, "Influence of strontium-rich pore-filling phase on the performance of La<sub>0.6</sub>Sr<sub>0.4</sub>CoO<sub>3-δ</sub> thin-film cathodes," *J. Power Sources*, **274**, 295-303 (2015).
- D. Sarantaridis and A. Atkinson, "Redox Cycling of Ni-Based Solid Oxide Fuel Cell Anodes: A Review," *Fuel Cells*, 7 [3] 246-258 (2007).
- T. Klemenso and M. Mogensen, "Ni-YSZ Solid Oxide Fuel Cell Anode Behavior Upon Reodx Cycling Based on Electrical Characterization," *J. Am. Ceram. Soc.*, **90** [11] 3582-3588 (2007).
- D. Fouquet, A.C. Muller, A. Weber, and E. Ivers-Tiffee, "Kinetics of Oxidation and Reduction of Ni/YSZ Cermets," *Ionics*, 9 [1-2] 103-108 (2003).
- B. Iwanschitz, L. Holzer, A. Mai, and M. Schütze, "Nickel agglomeration in Solid Oxide Fuel Cells under different operating conditions"; pp. 5-15 in *10<sup>th</sup> European SOFC Forum Proceedings, Chapter 08.* Edited by F. Lefebvre-Joud. European Fuel Cell Forum, Luzern, Switzerland, 2012.
- 9. A. Atkinson, S. Barnett, R. J. Gorte, J. T. S. Irvine, A. J. McEvoy, M. Mogensen, S. C. Singhal, and J. Vohs, "Advanced anodes for high-temperature fuel cells," *Nat. Mater.*, **3**, 17-27 (2004).
- 10. G. J. Nelson *et al.*, "Three-dimensional microstructural changes in the Ni–YSZ solid oxide fuel cell anode during operation," *Acta Mater.*, **60** [8] 3491-3500 (2012).
- N. Balakrishnan, T. Takeuchi, K. Nomura, H. Kageyama, and Y. Takeda, "Aging Effect of 8 mol % YSZ Ceramics with Different Microstructures," *J. Electrochem. Soc.*, **151** [8] A1286-A1291 (2004).
- M. Hattori, Y. Takeda, Y. Sakaki, A. Nakanishi, S. Ohara, K. Mukai, J.-H. Lee, and T. Fukui, "Effect of aging on conductivity of yttria stabilized zirconia," *J. Power Sources*, **126** [1-2] 23-27 (2004).

- J. R. Wilson *et al.*, "Three-dimensional reconstruction of a solid-oxide fuel-cell anode," *Nat. Mater.*, **5** [7] 541-544 (2006).
- P. R. Shearing, Q. Cai, J. I. Golbert, V. Yufit, C. S. Adjiman, and N. P. Brandon,
   "Microstructural analysis of a solid oxide fuel cell anode using focused ion beam techniques coupled with electrochemical simulation," *J. Power Sources*, **195** [15] 4804-4810 (2010).
- N. Vivet, S. Chupin, E. Estrade, T. Piquero, P. L. Pommier, D. Rochais, and E. Bruneton, "3D Microstructural characterization of a solid oxide fuel cell anode reconstructed by focused ion beam tomography," *J. Power Sources*, **196** [18] 7541-7549 (2011).
- N. Shikazono, D. Kanno, K. Matsuzaki, H. Teshima, S. Sumino, and N. Kasagi, "Numerical Assessment of SOFC Anode Polarization Based on Three-Dimensional Model Microstructure Reconstructed from FIB-SEM Images," *J. Electrochem. Soc.*, **157** [5] B665-B672 (2010).
- L. Holzer, B. Muench, B. Iwanschitz, M. Cantoni, T. Hocker, and T. Graule, "Quantitative relationships between composition, particle size, triple phase boundary length and surface area in nickel-cermet anodes for Solid Oxide Fuel Cells," *J. Power Sources*, **196** [17] 7076-7089 (2011).
- 18. L. Holzer *et al.*, "Microstructure degradation of cermet anodes for solid oxide fuel cells:
  Quantification of nickel grain growth in dry and in humid atmospheres," *J. Power Sources*, **196**[3] 1279-1294 (2011).
- Z. Jiao and N. Shikazono, "Simulation of Nickel Morphological and Crystal Structures Evolution in Solid Oxide Fuel Cell Anode Using Phase Field Method," *J. Electrochem. Soc.*, 161 [5] F577-F582 (2014).
- J. R. Wilson, J. S. Cronin, and S. A. Barnett, "Linking the microstructure, performance and durability of Ni-yttria-stabilized zirconia solid oxide fuel cell anodes using three-dimensional focused ion beam–scanning electron microscopy imaging," *Scr. Mater.*, 65 [2] 67-72 (2011).
- P. R. Shearing, J. Golbert, R. J. Chater, and N. P. Brandon, "3D reconstruction of SOFC anodes using a focused ion beam lift-out technique," *Chem. Eng. Sci.*, **64** [17] 3928-3933 (2009).
- J. R. Izzo, A. S. Joshi, K. N. Grew, W. K. S. Chiu, A. Tkachuk, S. H. Wang, and W. Yun, "Nondestructive Reconstruction and Analysis of SOFC Anodes Using X-ray Computed Tomography at Sub-50 nm Resolution," *J. Electrochem. Soc.*, **155** [5] B504-B5408 (2008).
- 23. K. N. Grew, Y. S. Chu, J. Yi, A. A. Peracchio, J. R. Izzo, Y. Hwu, F. De Carlo, and W. K. S.

Chiu, Nondestructive Nanoscale 3D Elemental Mapping and Analysis of a Solid Oxide Fuel Cell Anode," *J. Electrochem. Soc.*, **157** [6] B783-B792 (2010).

- F. Usseglio-Viretta, J. Laurencin, G. Delette, J. Villanova, P. Cloetens, and D. Leguillon, "Quantitative microstructure characterization of a Ni–YSZ bi-layer coupled with simulated electrode polarisation," *J. Power Sources*, **256**, 394-403 (2014).
- J. S. Cronin, Y. K. Chen-Wiegart, J. Wang, and S. A. Barnett, "Three-dimensional reconstruction and analysis of an entire solid oxide fuel cell by full-field transmission X-ray microscopy," *J. Power Sources*, 233, 174-179 (2013).
- 26. Y. Guan *et al.*, "Analysis of the three-dimensional microstructure of a solid-oxide fuel cell anode using nano X-ray tomography," *J. Power Sources*, **196** [4] 1915-1919 (2011).
- J. H. Jang, J. H. Ryu, and S. M. Oh, "Microstructure of Ni/YSZ cermets according to particle size of precursor powders and their anodic performances in SOFC," *Ionics*, 6 [1-2] 86-91 (2000).
- N. F. P. Ribeiro, M. M. V. M. Souza, O. R. Macedo Neto, S. M. R. Vasconcelos, and M. Schmal, "Investigating the microstructure and catalytic properties of Ni/YSZ cermets as anodes for SOFC applications," *Appl. Catal., A*, **353** [2] 305-309 (2009).
- 29. W. Guo and J. Liu, "The effect of nickel oxide microstructure on the performance of Ni–YSZ anode-supported SOFCs," *Solid State Ionics*, **179** [27-32] 1516-1520 (2008).
- T. Kawashima, S. Miyoshi, Y. Shibuta, and S. Yamaguchi, "Particle size dependence of polarization of Ni/YSZ cermet anodes for solid oxide fuel cells," *J. Power Sources*, 234, 147-153 (2013).
- M. Brown, S. Primdahl, and M. Mogensen, "Structure/Performance Relations for Ni/Yttria-Stabilized Zirconia Anodes for Solid Oxide Fuel Cells," *J. Electrochem. Soc.*, **147** [2] 475-485 (2000).
- X. Zhu, C. Guan, Z. Lü, and W. Su, "Effects of Initial Reduction Temperature on the Microstructures and Performances of Ni/YSZ Anodes for Solid Oxide Fuel Cells," *J. Electrochem. Soc.*, **160** [10] F1170- F1174 (2013).
- 33. K. N. Grew, A. A. Peracchio, A. S. Joshi, J. R. Izzo Jr., and W. K. S. Chiu, "Characterization and analysis methods for the examination of the heterogeneous solid oxide fuel cell electrode microstructure. Part 1: Volumetric measurements of the heterogeneous structure," *J. Power Sources*, **195** [24] 7930-7942 (2010).

- 34. G. Gaiselmann, M. Neumann, V. Schmidt, O. Pecho, T. Hocker, and L. Holzer, "Quantitative relationships between microstructure and effective transport properties based on virtual materials testing," *AIChE J.*, **60** [6] 1983–1999 (2014).
- 35. D. Wiedenmann *et al.*, "Three-dimensional pore structure and ion conductivity of porous ceramic diaphragms," *AIChE J.*, **59** [5] 1446-1457 (2013).
- 36. E. E. Petersen, "Diffusion in a pore of varying cross section," AIChE J., 4 [3] 343-345 (1958).
- L. Holzer, D. Wiedenmann, B. Muench, L. Keller, M. Prestat, P. Gasser, I. Robertson, and B. Grobéty, "The influence of constrictivity on the effective transport properties of porous layers in electrolysis and fuel cells," *J. Mater. Sci.*, 48 [7] 2934-2952 (2013).
- K. N. Grew, A. A. Peracchio, and W. K. S. Chiu, Characterization and analysis methods for the examination of the heterogeneous solid oxide fuel cell electrode microstructure: Part 2. Quantitative measurement of the microstructure and contributions to transport losses," *J. Power Sources*, **195** [24] 7943-7958 (2010).
- G. J. Nelson, A. A. Peracchio, and W. K. S. Chiu, "Analytical investigations of varying cross section microstructures on charge transfer in solid oxide fuel cell electrodes," *J. Power Sources*, **196** [10] 4695-4704 (2011).
- G. J. Nelson, B. N. Cassenti, A. A. Peracchio, and W. K. S. Chiu, "Two-dimensional charge transfer and space charge effects in extended surface solid oxide fuel cell electrodes," *J. Power Sources*, **205**, 48-56 (2012).
- M. B. Clennell, "Tortuosity: a guide through the maze"; pp. 299-344 in *Developments in Petrophysics, Geological Society Special Publication*. Edited by M.A. Lovell and P.K. Harvey. The Geological Society, London, 1997.
- O. Stenzel, O. Pecho, L. Holzer, M. Neumann, and V. Schmidt, "Predicting Effective Conductivities Based on Geometric Microstructure Characteristics," *AIChE J.*, submitted (2015).
- L. Holzer, B. Iwanschitz, Th. Hocker, L. Keller, O. Pecho, G. Sartoris, Ph. Gasser, and B. Muench, "Redox cycling of Ni–YSZ anodes for solid oxide fuel cells: Influence of tortuosity, constriction and percolation factors on the effective transport properties," *J. Power Sources*, **242**, 179-194 (2013).
- 44. B. Münch and L. Holzer, "Contradicting Geometrical Concepts in Pore Size Analysis Attained with Electron Microscopy and Mercury Intrusion," *J. Am. Ceram. Soc.*, **91** [12] 4059-4067

(2008).

- 45. B. Iwanschitz, "Degradation von Ni-Cermet-Anoden in keramischen Hochtemperaturbrennstoffzellen (Degradation of Ni-Cermet-anodes in solid oxide fuel cells (SOFC))"; PhD Thesis, RWTH Aachen University, Germany, 2012.
- B. Iwanschitz, J. Sfeir, A. Mai, and M. Schütze, "Degradation of SOFC Anodes upon Redox Cycling: A Comparison Between Ni/YSZ and Ni/CGO," *J. Electrochem. Soc.*, **157** [2] B269-B278 (2010).
- 47. E. W. Washburn, "The Dynamics of Capillary Flow," Phys. Rev., 17, 273-283 (1921).
- 48. S. Diamond, "Mercury porosimetry: An inappropriate method for the measurement of pore size distributions in cement-based materials," *Cem. Concr. Res.*, **30** [10] 1517-1525 (2000).
- 49. K. Thulasiraman and M. N. S. Swamy, *Graphs: Theory and Algorithms*. John Wiley & Sons, NewYork, 1992.
- A. Wiegmann and A. Zemitis, "EJ-HEAT: A Fast Explicit Jump Harmonic Averaging Solver for the Effective Heat Conductivity of Composite Materials," Report of the Fraunhofer ITWM, Nr. 94, 2006.
- B. Hua, W. Zhang, M. Li, X. Wang, B. Chi, J. Pu, and J. Li, "Improved microstructure and performance of Ni-based anode for intermediate temperature solid oxide fuel cells," *J. Power Sources*, 247, 170-177 (2014).
- 52. A. Buyukaksoy, V. Petrovsky, and F. Dogan, "Optimization of Redox Stable Ni-YSZ Anodes for SOFCs by Two-Step Infiltration," *J. Electrochem. Soc.*, **159** [12] F841-F848 (2012).
- T. Fukui, S. Ohara, and K. Mukai, "Long-Term Stability of Ni-YSZ Anode with a New Microstructure Prepared from Composite Powder," *Electrochem. Solid-State Lett.*, **1** [3] 120-122 (1998).
- M. Pihlatie, A. Kaiser, P. H. Larsen, and M. Mogensen, "Dimensional Behavior of Ni–YSZ Composites during Redox Cycling," *J. Electrochem. Soc.*, **156** [3] B322-B329 (2009).
- 55. T. Hocker, B. Iwanchitz, and L. Holzer, "Assessing the effect of electrode microstructure on repeat unit performance and cell degradation"; presented at ModVal 7, 7th Symposium on fuel cell modeling and experimental validation, Morges, Switzerland, March 23-24, 2010.

Table 1. Summary of degradation phenomena in Ni and YSZ upon redox cycling of fine and coarse anodes.

		FINE	COA	RSE
	Ni	YSZ	Ni	YSZ
Before redox cycling (initial)	(+) High initial e- conductivity	(+) High initial ionic conductivity	(-) Low initial e- conductivity	(-) Low initial ionic conductivity
After redox cycling (degradation)	(-) Strong coarsening, (-) Loss of percolation, (-) Increase of $ au$	<ul> <li>(+) Strong bottlenecks due to high sinter activity,</li> <li>(+) Small increase of T</li> </ul>	(-) Significant coarsening but (+) Low loss of percolation and Low change of $ au$ and $eta$	(-) Weak bottlenecks due to low sinter activity, (-) High loss of percolation, (-) Strong change of $ au$ and $eta$

# **Supplementary Information**



Figure S1. Representative c-PSD (solid lines) and MIP-PSD (dashed lines) before and after redox cycling. The c-PSD curves reflect the size of the bulges and the MIP-PSD curves reflect the size of the bottlenecks. (A) The shift in the c-PSD curve of Ni in fine sample after redox cycling illustrates the increase in the average size of the bulges while the MIP-PSD shows that the bottlenecks oft he Ni hardly change. (B) The YSZ bulges expand and the bottlenecks shrink in coarse sample as illustrated in the corresponding shifts in c-PSD and MIP-PSD curves.

		Pixel size (nm)		Slice thickness (nm)	Pixel matrix		Nr of slices	Total nr of voxels	Size of image window (µm)		Total (µm³)	
		x	У	z	x	У	z		x	У	z	
	Fine	19.53	19.53	20.00	995	1'304	733	951'052'840	19.43	25.47	14.66	7'255.03
Before redox	Medium	24.41	24.41	25.00	960	1'110	610	650'016'000	23.43	27.10	15.25	9'682.77
	Coarse	29.14	29.14	30.00	744	1'417	456	480'737'088	21.68	41.29	13.68	12'246.39
	Fine	19.53	19.53	20.47	1'171	1'343	461	724'993'033	22.87	26.23	9.44	5'660.52
After redox	Medium	17.90	17.90	25.00	1'318	1'520	459	919'542'240	23.60	27.21	11.48	7'368.73
	Coarse	17.90	17.90	25.00	1'368	1'630	500	1'114'920'000	24.49	29.18	12.50	8'934.38

Table S1. Summary of image data for 3D quantitative microstructure analyses of Ni-YSZ anodes before and after redox cycling.

Table S2. Summary of image data for 3D analyses of simulated M-factors ( $M_{sim}$ ) on geodict.

		Pixel matrix		Nr of slices	
		x	У	Z	
Before redox	FINE	500	500	500	
	MEDIUM	500	500	500	
	COARSE	500	500	456	
After redox	FINE	500	500	461	
	MEDIUM	1000	1000	459	
	COARSE	1000	1000	500	

	Before redox cycling			After redox cycling			
Ni	FINE	MEDIUM	COARSE	FINE	MEDIUM	COARSE	
$\phi$	0.322	0.250	0.229	0.222	0.233	0.244	
Р	0.985	0.965	0.959	0.809	0.884	0.886	
$\phi_{\rm eff}$ = $\phi^* P$	0.317	0.241	0.220	0.179	0.206	0.216	
β	0.275	0.260	0.220	0.188	0.345	0.372	
τ	1.219	1.341	1.605	1.375	1.358	1.673	
<i>M</i> <sub>pred</sub>	0.071	0.033	0.011	0.019	0.029	0.011	
YSZ	FINE	MEDIUM	COARSE	FINE	MEDIUM	COARSE	
$\phi$	0.421	0.388	0.384	0.312	0.376	0.324	
Р	0.999	0.986	0.923	0.961	0.869	0.184	
$\phi_{\rm eff} = \phi^* P$	0.421	0.383	0.354	0.300	0.327	0.060	
β	0.367	0.095	0.007	0.088	0.042	0.0001	
τ	1.108	1.176	1.889	1.430	1.353	1.100	
$M_{ m pred}$	0.173	0.071	0.002	0.020	0.022	0.001	
Pore	FINE	MEDIUM	COARSE	FINE	MEDIUM	COARSE	
$\phi$	0.254	0.362	0.387	0.466	0.390	0.432	
Р	0.988	0.998	0.999	0.999	0.998	0.992	
$\phi_{\rm eff}$ = $\phi^* P$	0.251	0.361	0.386	0.466	0.389	0.428	
β	0.271	0.550	0.563	0.547	0.594	0.487	
τ	1.324	1.110	1.103	1.073	1.081	1.082	
<b>M</b> <sub>pred</sub>	0.037	0.170	0.190	0.260	0.216	0.220	

# Table S3. Summary of transport-relevant microstructure parameters and the predicted M-<br/>factors ( $M_{pred}$ ) obtained using Eq. 4.

#### **List of Figures**

Figure 1. 3D microstructures (FIB-tomography) of Ni-YSZ anodes with increasing coarseness from left to right. Top row is before and bottom row after redox cycling at 950°C. Pores (black), YSZ (gray) and Ni (white). Significant Ni agglomeration is visible in all samples after redox cycling.

Figure 2. 2D-slices of segmented 3D images of all the Ni-YSZ samples investigated in this study. Three different YSZ powders (fine, medium, and coarse) are used for composite anode fabrication. In the initial microstructures (top row), Ni (white) and pores (black) follow the size of the YSZ (gray) starting particle size. Redox cycling (bottom row) leads to significant coarsening and agglomeration of Ni.

Figure 3. Evolution of electrical conductivities ( $\sigma_{eff}$ ) of Ni-YSZ during exposure to 8 redox cycles at 950°C based on the work of Iwanschitz.<sup>45</sup> Linear trends of degradation are observed between the 1<sup>st</sup> and 8<sup>th</sup> cycles.  $\sigma_{eff}$  of the fine anode is strongly degrading. In the medium-grained anode  $\sigma_{eff}$  is slightly decreasing. In the coarse anode,  $\sigma_{eff}$  is even improving. The differences in the initial values and in the curing behavior during the 1<sup>st</sup> cycle are not well understood.

Figure 4. Porosity ( $\varepsilon$ ) in Ni-YSZ anodes. In fresh samples, porosity increases from fine to coarse. After sintering the fine anode is relatively dense. Redox cycling then leads to a significant increase of porosity in the fine anode.

Figure 5. (A) Percolation factors (*P*) of the different phases and (B) solid volume fractions ( $\phi_{eff}$ ) in the 6 Ni-YSZ anodes. *P* describes the interconnected portion of a phase. (A) After redox cycling the percolation factors of YSZ decrease significantly in the coarse anode. The percolation factors of Ni decrease only moderately (-10 to -20 %). (B) The ratio Ni:YSZ is similar in all six samples (40:60 vol%), however the effective volume fractions (interconnected portions) of YSZ and Ni show partially strong variations upon redox cycling due to changes of P (e.g. YSZ coarse and Ni fine).

Figure 6. (a) Average sizes of bulges ( $r_{50,max}$  from c-PSD), (b) bottlenecks ( $r_{50,min}$  from MIP-PSD) and (c) constriction factors ( $\beta_{Ni}$ ) for Ni in composite anodes, before (black) and after redox cycling (gray). The  $\beta_{Ni}$  in the fine sample decreases due to the growth of bulges ( $r_{50,max}$   $\bigstar$ ) while the  $\beta_{Ni}$  in medium and coarse samples increase due to the widening of bottlenecks ( $r_{50,min}$   $\bigstar$ ).

Figure 7. (a) Average sizes of bulges ( $r_{50,max}$ ), (b) bottlenecks ( $r_{50,min}$ ) and (c) constriction factors ( $\beta_{YSZ}$ ) of YSZ in composite anodes, before (black) and after redox cycling (gray). Upon redox cycling, the sizes of the bulges remain nearly constant while the bottlenecks are shrinking ( $r_{50,min} \Psi$ ). Consequently, all the  $\beta_{YSZ}$  decrease after redox cycling.

Figure 8. (a) Average sizes of bulges ( $r_{50,max}$ ), (b) bottlenecks ( $r_{50,min}$ ) and (c) constriction factors ( $\beta_{Pore}$ ) for the pores in Ni-YSZ anodes, before (black) and after redox cycling (gray). For medium and coarse

all parameters remain stable during redox cycling. In the fine sample the bottlenecks expand ( $r_{50,min}$   $\uparrow$ ), which results in a higher  $\beta_{Pore}$  after redox cycling.

Figure 9. Mean geodesic tortuosity of (a) Ni, (b) YSZ and (c) Pore before (black) and after redox cycling (gray). Note: Geodesic tortuosities are usually relatively low (i.e. < 1.5) and represent the shortest pathways from A to B (in a predetermined direction) through the voxel-domain of a segmented phase.

Figure 10. Simulated M-factors ( $M_{sim}$ ) of (a) Ni and (b) YSZ before (black) and after (gray) redox cycling for fine, medium and coarse samples. Pristine samples exhibit a decreasing  $M_{sim}$  from fine to coarse for Ni and YSZ. After exposure to redox cycling, the  $M_{sim}$  of Ni in fine decreases while it improves in medium and coarse.  $M_{sim}$  of YSZ in all samples decreases after redox cycling.

Figure 11. (a,b) Summary of  $M_{\text{pred}}$  ( $\approx M_{\text{sim}}$ ) and (c,d) topological parameters in pristine samples of fine, medium and coarse anodes. The M-factor of Ni is significantly affected by tortuosity, while the M-factor of YSZ is strongly affected by both, tortuosity and constrictivity.

Figure 12. Comparison between predicted ( $M_{pred}$ ) and simulated ( $M_{sim}$ ) microstructure factors of Ni and YSZ in pristine anodes (a, b) and after redox cycling (c,d). Before redox cycling, the data points lie close to the diagonal reference line (solid line), which confirms a strong correlation between the  $M_{pred}$  and  $M_{sim}$ . (c) After redox cycling, the data points for the Ni fine anode lie close to reference line, whereas the data points of medium and coarse anodes are clearly off the diagonal reference line (weak correlation between the  $M_{pred}$  and  $M_{sim}$ ).

Figure 13. (a,b) Profiles of effective volume fraction ( $\phi P = \phi_{\text{eff}}$ ) and (c,d) geodesic tortuosity ( $\tau$ ) in the fine anode as a function of the film thickness (x-direction). Note: Connectivity check is performed with the inlet plane on the left side (Distance 0). Connected volume fractions of Ni and YSZ in the fine sample vary in a narrow range. The effective (connected) volume fractions are slightly lower in samples after redox cycling, due to loss of percolation and swelling. Geodesic tortuosity lies between 1.1 and 1.35 before redox cycling, while higher (1.35 – 1.8) and more fluctuating tortuosities are observed after redox cycling.

Figure 14. (a,b) Profiles of connected volume fraction ( $\phi P = \phi_{eff}$ ) and (c,d) tortuosity ( $\tau$ ) of Ni and YSZ in medium and coarse samples, respectively as a function of film thickness (x-direction). Connectivity check is performed with the inlet plane (left side). The fluctuating values for YSZ are attributed to significant loss of connectivity, which is particularly strong after redox cycling (Compare Fig. 5). Geodesic tortuosities are more fluctuating (values between 1- 2.5) as compared to the fine sample.

Figure 15. (Left) Comparison between  $M_{pred}$  and  $M_{sim}$  for Ni, illustrating the effect of varying image window size. The point represented by a star (\*) is obtained if both  $M_{pred}$  and  $M_{sim}$  are obtained by analysis of the same image window (region B, right image). The data point marked with an open

triangle ( $\Delta$ ) is obtained if  $M_{\text{pred}}$  is based on analysis of region A (right) while  $M_{\text{sim}}$  was obtained from region B (right). Note: The image on the right is a 2D-cross section of a 3D image window. The larger image window (A, in 3D) exceeds the limits of conventional voxel based computations ( $M_{\text{sim}}$ ) but can be used for topology analysis ( $M_{\text{pred}}$ ).

Figure 16. Relative experimental conductivities (open symbols) for fine, medium and coarse anodes and their evolution over 8 redox cycles at 950°C based on the work of lwanschitz.<sup>45</sup> Relative experimental conductivity means that the measured conductivity after x cycles is normalized by the conductivity measured after the 1<sup>st</sup> cycle. The relative predicted conductivity (filled symbols) is based on the  $M_{pred}$ , with normalization by the initial values (0 cycles). Similar evolution curves are obtained by prediction and experiment.

Figure 17. Redox degradation of the fine anode is described with normalized M-factors and topological parameters of Ni and YSZ. Normalization means building the ratio of values before over values after redox cycling. The degradation of the Ni M-factor is significantly affected by changes in volume fraction (i.e. percolation) and tortuosity, whereas the degradation of the YSZ M-factor is most significantly affected by changes in tortuosity. The exponents of the microstructural parameters are those from Eq. 4, which allows to directly assessing the relative roles of these terms on the M-factors.

Figure 18. Illustration of redox degradation by normalized M-factors and topological parameters for Ni in the coarse anode (i.e. ratio of values before/after redox). Upon redox cycling the M-factor (Ni, coarse) and associated electrical conductivity do not degrade, since the effect of worsened tortuosity (normalized  $\tau^{-5.17}$  <1) is compensated by improved constrictivity (normalized  $\beta^{0.36}$  >1). The exponents of the microstructural parameters are those from Eq. 4, which allows to directly assessing the relative roles of these terms on the M-factors.

Figure 19. Different modes of Ni agglomeration and growth in Ni-YSZ anodes during redox cycling. In the fine anode (a) where particles are more granular, Ni growth is mainly located around the Ni bulges. In the coarser anode (b) Ni forms irregularly shaped domains (not round particles), and growth is often located at the bottlenecks (i.e. at concavities with relatively high surface energy).

Figure 20. 3D visualization of YSZ (top), Ni (middle) and Ni + YSZ (bottom) in coarse sample before (left) and after (right) redox cycling. Redox degradation invokes a splitting of YSZ particles and disintegration into numerous disconnected islands (top). Ni agglomeration leads to the formation of a less granular structure (middle). Ni is partially overgrowing the small, disconnected YSZ islands (bottom).

Figure 21. Relative conductivities of anodes fabricated with mixed powders (i.e. 50%/50% finemedium and 50%/50% fine-coarse, respectively) compared to fine, medium and coarse.<sup>45</sup> The 'mixed anodes' show a similar behavior as the fine anode, which indicates that the fraction of fine powders is too high.



Figure 1



Figure 2



Figure 3



Figure 4



Figure 5



Figure 6



Figure 7



Figure 8



Figure 9







Figure 11



Figure 12



Figure 13



Figure 14



Figure 15



Figure 16







Figure 18



Region of Ni growth

Figure 19



Figure 20



Figure 21